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Process for the catalyst-free preparation of cyanophenols from methoxybenzonitriles

Description

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The present invention provides a process for the catalyst-free preparation of cyanophenols.

for industrially established process preparing phenols which is described in detail in the 10 H.-J. Arpe, Industrielle literature [K. Weissermel, organische Chemie [Industrial organic chemistry], 3rd revised and extended edition, VCH Weinheim, 1988, p. 376] is the known conversion of an isopropylaromatic and the subsequent conversion to the 15 using oxygen phenol and acetone (Hock phenol synthesis). process are the equimolar Disadvantages of this occurrence of acetone and the high consumption of propene to prepare the isopropylaromatic. In addition, it is not possible to prepare arbitrarily substituted 20 cyanophenols by this process.

In the already classic process [K. Weissermel, H.-J. Arpe, Industrielle organische Chemie [Industrial organic chemistry], 3rd revised and extended edition, VCH Weinheim, 1988, p. 370] for preparing phenols from benzenesulfonic acids, large amounts of salts (Na2SO3, Na2SO4) are obtained as a coproduct, so that the process can no longer be used in the western world for environmental reasons.

preparation of phenols from chloroaromatics means of NaOH is also known from the literature and has been industrially realized [K. Weissermel, H.-J. Arpe, Industrielle organische Chemie [Industrial organic 35 revised and extended edition, VCH chemistry], 3rd Weinheim, 1988, p. 372], but in particular the necessary, sometimes drastic reaction conditions and

particularly the temperatures above 360°C are regarded as disadvantageous. A conversion of the process to substituted phenols, for example cyanophenols, is not possible owing to the required reaction conditions.

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The preparation of cyanophenols by the formation of the cyano unit is likewise well known and described. For instance, the cyano function may be formed from the corresponding aromatic aldehydes with hydroxylamine and auxiliary reagents, or else from aldehydes with ammonia 10 and auxiliary reagents, for which a wide variety of processes are used. [A. K. Chakraborti et al., Indian Journal of Chemistry, Section B: (2001), 40B(10), 1000-1006; B. Das et al., Synlett (2000), (11), 1599-1600; (2001),(2), al., Synlett 15 G. Lai et A. R. Bajpai et al., Synthetic Communications (2000), 2785-2791; A. S. Paraskar et al., Res., Synop. (2000), (1), 30-31; A. K. Chakraborti, Tetrahedron (1999), 55(46), 13265-13268; H. M. Kumar et al., Synthesis (1999), (4), 586-587; G. Sabitha et al., 20 Synth. Commun. (1998), 28(24), 4577-4580; E. Wang et Lett. (1998), 39(23), 4047-4050; Tetrahedron H. M. Meshram, Synthesis (1992), (10), 943-4; D. Konwar al., Tetrahedron Lett. (1990), 31(7), 1063-4; P. Capdevielle et al., Synthesis (1989), (6), 451-2; 25 G. Jin et al., (1985), 21(3), 506-8; J. C. Vallejos et al., FR 2 444 028; H. Schlecht, DE 20 14 984].

Even though these processes sometimes result in good to very good yields, the use of the expensive aromatic 30 aldehydes is to be regarded as disadvantageous in every case. In addition, the use of the readily decomposing and/or the use of ammonia hydroxylamine expensive and usually environment-endangering auxiliary reagents is necessary. The possible alternative of 35 microwave irradiation is technically demanding and also too expensive.

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It is likewise known to form a nitrile function from the corresponding acids and ammonia using dehydrating agents and at high temperatures, although the raw materials and the extreme reaction conditions are an obstacle to wide use.

Also known from the literature is the ammoxidation of the corresponding cyanophenols methylphenols to [M. V. Landau et al., Applied Catalysis A: General (2001), 208(1,2), 21-34; A. Martin et al., J. Prakt. 10 Chem. (1990), 332(4), 551-6; H. Bruins Slot, DE 20 37 9451, which succeeds, though, in only very modest vields. Disadvantages of this process are not only the low yield but also the high cost of inconvenience for the industrial synthesis. The same applies for the 15 formation of the nitrile function from a benzoic acid and ammonia or from an ester and ammonia, according to the following references [R. Ueno et al., EP 74 116; M. Araki et al., JP 53040737; R. Perron, FR 2 332 261; G. Bakassian, M. Lefort, DE 22 05 360; H. Eilingsfeld, 20 20 20 866; T. Ichii et al., DE E. Schaffner, 43029944].

The literature also gives details on the ether cleavage form phenols [P. R. Brooks et al., Journal 25 Organic Chemistry (1999), 64(26), 9719-9721]. In this process, especially the stoichiometric use expensive raw materials boron trichloride and the use of large amounts of n-butylammonium iodide are regarded 30 as disadvantageous.

Systems which have been developed specifically for the cleavage of allyl ethers are also described in the present context. To this end, it is possible to use systems composed of CeCl3 and Nal [R. M. Thomas et al., Tetrahedron Letters (1999), 40(40), 7293-7294] or NaBH4 [R. M. Thomas et al., Tetrahedron Lett. (1997), 38(26), 4721-4724], else electrochemical processes or

[D. Franco et al., Tetrahedron Lett. (1999), 40(31), 5685-5688; A. Yasuhara et al., J. Org. Chem. (1999), 64(11), 4211-4213; K. Fujimoto et al., Tetrahedron (1996), 52(11), 3889-96; S. Olivero et al., J. Chem. Soc., Chem. Commun. (1995), (24), 2497-8]. However, the latter process variant is expensive and it requires the use of heavy metals; in addition, this process variant is restricted exclusively to the allyl ethers which are difficult to synthesize.

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The preparation of nitrophenols from nitroaromatics by substituting hydrogen with hydroperoxide anions in the presence of strong bases is a very interesting process, but is unfortunately restricted to nitroaromatics; in addition, it is necessary to use liquid ammonia and readily decomposable and thus dangerous hydroperoxides [M. Makosza et al., J. Org. Chem. 1998, 63, 4199-4208]. To prepare cyanophenols, the nitro group has to be converted to a cyano group in a complicated manner.

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T. Senba and K. Sakano (JP 09023893) and H. Semba et al. describe the enzymatic synthesis of phenols [Appl. Microbiol. Biotechnol. 1996, 46, 432-437]. However, the low space-time yields and the long reaction times mean that this process cannot be utilized in an economic manner.

The synthesis of phenols from anilines by diazotization and decomposition of the diazonium compound in the presence of metals, particularly copper salts, has also been known for some time. Even though more recent optimize the studies have attempted to process al., EP596 684], this [B. C. Gilbert et nevertheless always leads via a diazonium compound which is difficult to handle.

According to S. Prouilhac-Cros et al., the preparation from arylsilanes with of phenols H2O2 and

stoichiometric amounts of fluoride leads to phenols in good yields [Bull. Soc. Chim. Fr. 1995, 132, 513-16]. However, the arylsilane required is not sufficiently available in industrial quantities.

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The synthesis of phenols from aryl methyl ethers with ethanethiolates is restricted to laboratory applications [J. A. Dodge et al., J. Org. Chem. 1995, 60, 739-41]. For industrial syntheses, the reaction is sulfur and malodorous because toxic unsuitable compounds are obtained.

The cleavage of aryl methyl ethers with the FeO/glacial acetic acid/oxygen system has likewise been described [A. F. Duprat et al., J. Mol. Catal. 1992, 77]. This 15 particularly activated process is restricted to aromatics and gives the desired products only in low to very low yields. Only slightly better yields in the cleavage of aryl methyl ethers are obtained with AlCl3/NaCl [G. Adamska et al., Biul. Wojsk, Akad. Tech. 20 1980, 29, 93-99]. The large amounts of inorganic waste which form at the same time do not allow any industrial application of the process. The AlCl3/Ni system which is described in the literature for the cleavage of 25 these ethers also does not offer any advantages whatsoever, since temperatures above 240°C and long reaction times are required [H. Kashiwagi, S. Enomoto, Yakuqaku Zasshi 1980, 100, 668-71].

A very complicated process for the cleavage of aryl 30 methyl ethers and for the preparation of hydroxybenzonitrile is transmethylation (for example FR 1 565 812), in which the reaction of methoxybenzonitrile with the sodium salt of cresol to the sodium salt of hydroxy-35 benzonitrile and methoxycresol is effected temperatures above 200°C. This process affords large amounts of waste and has a very complicated procedure. Although aryl methyl ethers in principle constitute very suitable raw materials, the cleavage of the ether is very difficult; alternative cleavage processes are not available.

All processes mentioned lead to the desired products and have also already been used successfully for a large number of highly varying applications. However, all of these processes for preparing phenols especially cyanophenol have the disadvantage that they have a very complicated procedure, that expensive raw 10 materials have to be used, that large amounts of waste are formed or that the yield is only very low.

It is therefore an object of the present invention to develop a process for the catalyst-free preparation of 15 cyanophenols, which allows the environmentally friendly and low-waste preparation of the desired product with low priced raw materials in high yields. In particular, the use of heavy metals, as is customary, for example, when metals are used as the catalyst, should be 20 dispensed with.

This object is achieved by a corresponding process, in which a substituted methoxybenzonitrile of the general 25 formula (I)

where

are each independently hydrogen, a 30 R1, R2, R3 and R4 C1-10-alkyl, C2-8-alkoxy, aryl, phenoxy or a further nitrile group

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reacted with an alkali metal alkoxide at is temperatures between 80 and 230°C.

It has been found, surprisingly, that not only is it possible, as desired, to dispense fully with catalysts for the performance of the reaction, and that the cyanophenols are obtained in very good yields and purities, but also that a relatively simple process which can be performed without the occurrence of byproducts on the industrial scale without any problems 10 is thus available.

The selection of the aromatic raw materials is not restricted only to simple methoxybenzonitriles, rather also includes substituted methoxybenzonitriles, and in particular di-, tri-, tetra- or pentamethoxybenzonitriles are suitable.

Preferred alkali metal alkoxide components are methoxides and, among these, in particular sodium 20 methoxide.

The process according to the invention can be carried relatively large temperature range. within a However, particularly suitable reaction temperatures have been found to be between 120 and 200°C and most preferably between 140 and 180°C.

Typically, the reaction succeeds at best when the molar ratio of the methoxybenzonitrile component to the 30 alkali metal alkoxide component is from 1:0.5 to 1.5 and more preferably 1:1.0 to 1.1.

Typically, the present process succeeds even without presence of a solvent. However, the present 35 invention also provides for the use of a suitable solvent, for which either polar or nonpolar solvents may be used. Particular preference is given to C1-65

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alcohols, for example methanol, and/or a solvent from the group of tetrahydrofuran, benzene, toluene, xylene and methyl tert-butyl ether. Especially suitable for practical reasons and for reasons of cost is the use of simple alcohols, for example methanol.

The preferred reaction is typically carried out by initially charging the alkoxide component in an alcohol (for example sodium methoxide in methanol), then adding the methoxybenzonitrile component, which is preferably stirring; this should preferably be effected with effected in an autoclave, in which case the mixture is heated to the required reaction temperature and this is maintained until the desired conversion has attained.

The sequence of addition of the starting materials is not restricted to this preferred sequence. Instead, it is also possible to carry out the reaction with a sequence the of different addition components. The addition of the individual components, addition of the methoxybenzonitrile especially the component to the alkoxide, can also be graduated over a prolonged period during the reaction, or else be continuous.

The required aromatic raw materials, the methoxybenzonitriles, may, according to the prior art, also be prepared by ammoxidation in a simple, environmentally friendly and virtually waste-free manner from the corresponding methoxytoluenes and in the presence of ammonia and (atmospheric) oxygen, which the present invention regards as a particularly suitable process variant.

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The present invention also provides for the methoxybenzonitrile component not being isolated, but rather being reacted directly in the context of the invention.

The novel process according to the invention thus allows the catalyst-free preparation of cyanophenols from methoxybenzonitriles with high yields and thus also a guaranteed small amount of waste.

The present process additionally describes for the first time a process for preparing cyanophenols which starts from simple, inexpensive and readily available raw materials, and proceeds under industrially readily realizable conditions.

Examples

Example 1 15

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26.6 g of anhydrous 4-methoxybenzonitrile were added to 39.6 g of 30% methanolic anhydrous sodium methoxide solution and heated to 175°C with stirring at a start pressure of 5 bar of nitrogen in an autoclave. After 8 hours, the mixture was cooled, then 100 ml of water 20 were added and only a small amount of solid (< 0.1 g) was filtered off. Under cold conditions, sufficient 32% hydrochloric acid was then added to the filtrate to attain a pH of 2. After 60 min, the precipitate formed drying, off. After 20 g 25 filtered was 4-cyanophenol product were obtained. (84.1% of theory).

Example 2

26.6 g of anhydrous 4-methoxybenzonitrile were added to 54 g of 30% methanolic anhydrous sodium methoxide 30 solution and heated to 155°C with stirring at 5 bar of nitrogen as the start pressure in an autoclave. After hours, the mixture was cooled, then 90 ml of methanol and 80 ml of water were added and only a small amount of solid (< 0.1 g) was filtered off. Under cold 35 conditions, sufficient 32% hydrochloric acid was then added to the filtrate to attain a pH of 2. After 60 min, the precipitate formed was filtered off. After

drying, 20.2 g of the 4-cyanophenol product were obtained. (84.9% of theory).

Example 3

18.8 g of anhydrous 4-methoxybenzonitrile were added to 5 49 g of 25% methanolic anhydrous sodium methoxide solution and heated to 140°C with stirring at a start pressure of 5 bar of nitrogen as the start pressure in an autoclave. After 8 hours, the mixture was cooled and then 162 ml of water were added. Under cold conditions, 10 sufficient 32% hydrochloric acid was then added to attain a pH of 2. After 60 min, the precipitate formed off. After drying, 15 g of filtered was 4-cyanophenol product were obtained. (89.3% of theory).

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Example 4

26.6 g of anhydrous 4-methoxybenzonitrile were added to 97.2 g of 21% ethanolic anhydrous sodium methoxide solution and heated to 160°C with stirring in an autoclave. After 8 hours, the mixture was cooled and then 162 ml of water were added. Under cold conditions, sufficient 32% hydrochloric acid was then added to the filtrate to attain a pH of 2. After the precipitate formed had been filtered off and after drying, 4.8 g of the 4-cyanophenol product were obtained. (19.3% of theory).

Example 5

18.8 g of anhydrous 2-methoxybenzonitrile were added to
49 g of 25% methanolic anhydrous sodium methoxide
solution and heated to 140°C with stirring at a start
pressure of 5 bar of nitrogen in an autoclave. After 8
hours, the mixture was cooled and then 162 ml of water
were added. Under cold conditions, sufficient 32%
35 hydrochloric acid was then added to attain a pH of 2.
After the precipitate formed had been filtered off and
after drying, 16.8 g of the 2-cyanophenol product were
obtained. (100%).